



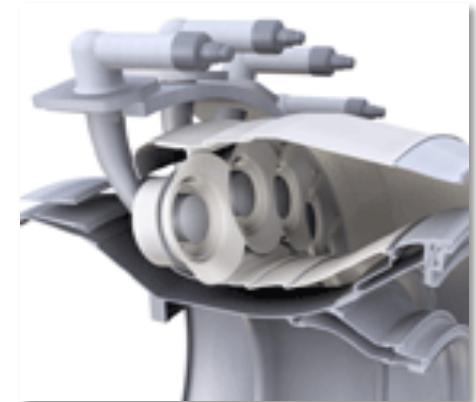
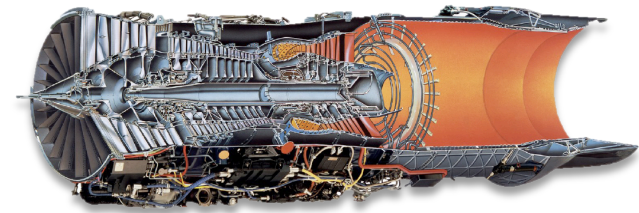
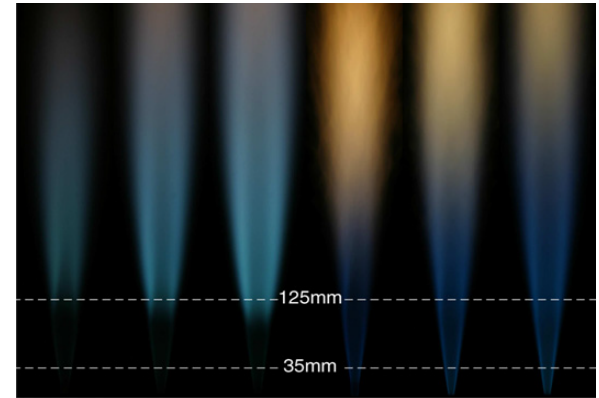
Turbulent Flames and the Role of Chemistry

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Sponsor: ONR, AFOSR, DoE

Motivation

- Advanced combustion strategies rely on
 - Low/moderate temperature combustion
 - High-pressure operating conditions
 - (Ultra)Lean and stratified combustion
 - Emerging and alternative fuel combustion
- Challenges
 - Shift from mixing-controlled to kinetics-controlled combustion regime
 - Increasing relevance of **ignition-kinetics** and low-temperature chain-branching reactions
 - Increasing **significance of turbulence** and turbulence/chemistry interaction
 - Finite-rate chemistry effects
 - Operation near stability limit





Motivation

- Objective
 - Development of high-fidelity combustion for prediction of turbulent reacting flows under consideration of
 - Finite-rate chemistry
 - Turbulence/chemistry coupling
 - Transient combustion-dynamical processes
- Relevance
 - Identify and isolate combustion-physical processes
 - Combustor-design, control, and optimization
 - Guide experimental instrumentation



Overview

- Motivation
- LES-combustion modeling
 - Flamelet-based formulation
- **Part 1:** Modeling and simulation of combustion-physical processes: LES of lifted vitiated flames
- **Part 2:** Guide experimental instrumentation: Turbulent inhomogeneities and facility-effects?
- Summary and conclusions

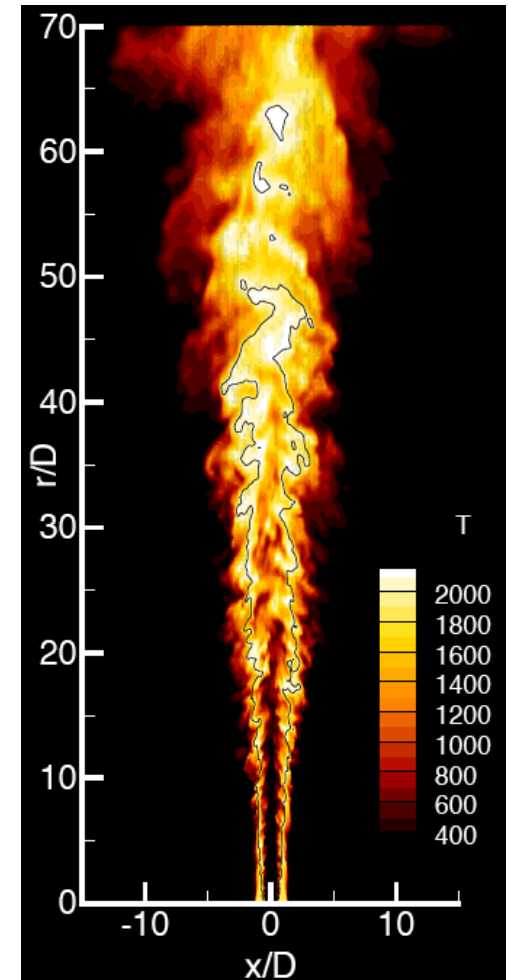


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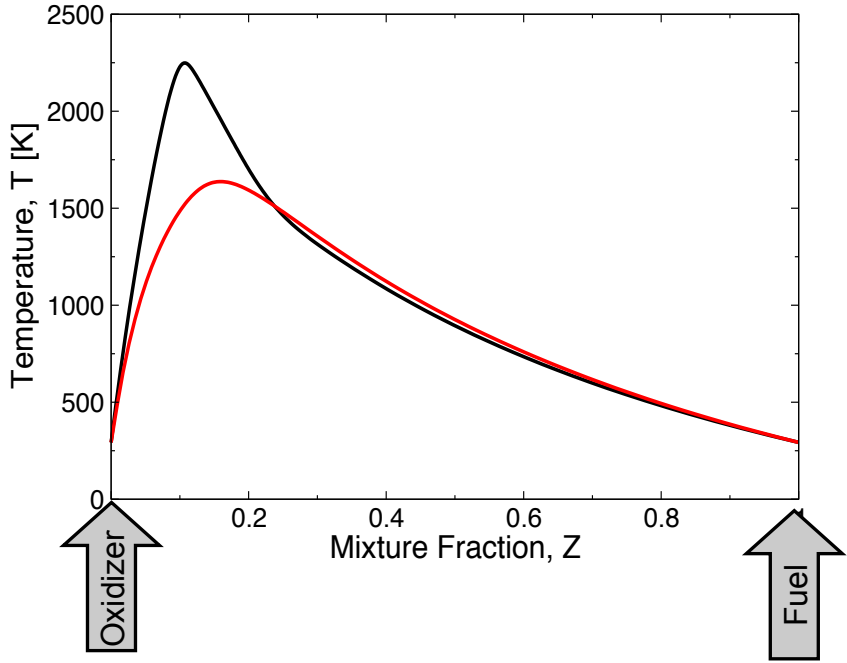
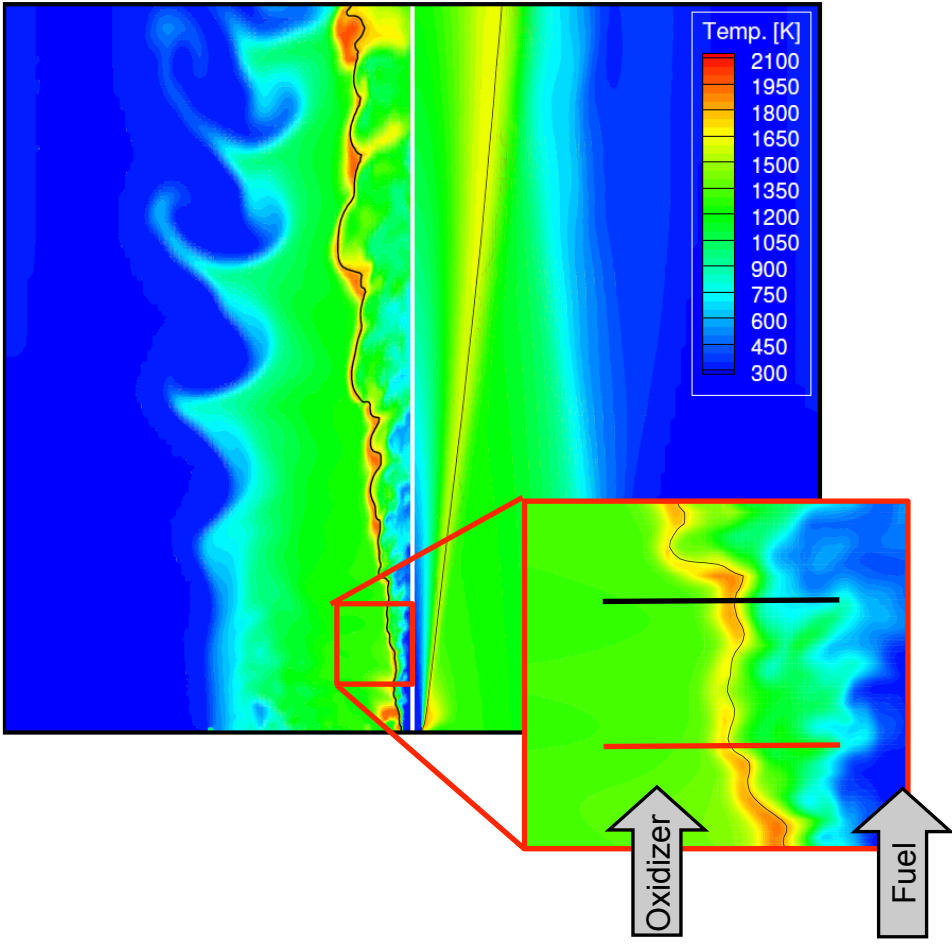
LES Combustion Modeling

- LES Flamelet-based combustion models
 - Representation of turbulent flame as **unsteady reaction-diffusion layer** that is embedded in turbulent flame
 - Interaction of flame structure with turbulent environment leads to **stretching, deformation, and extinction** of flame



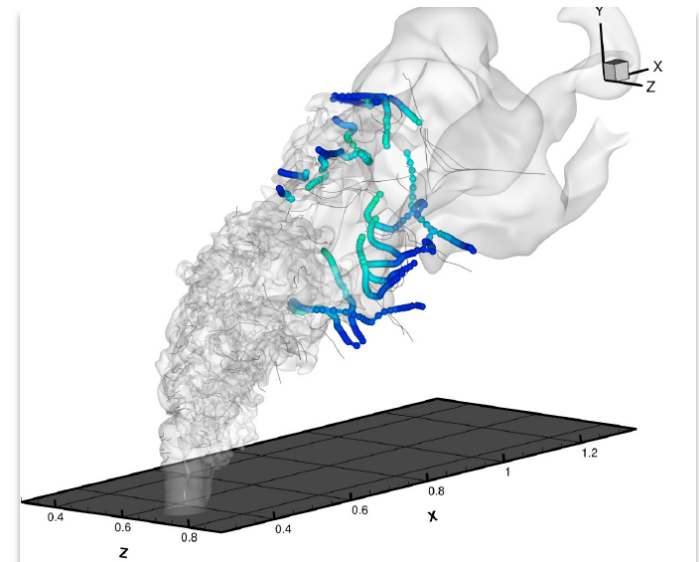
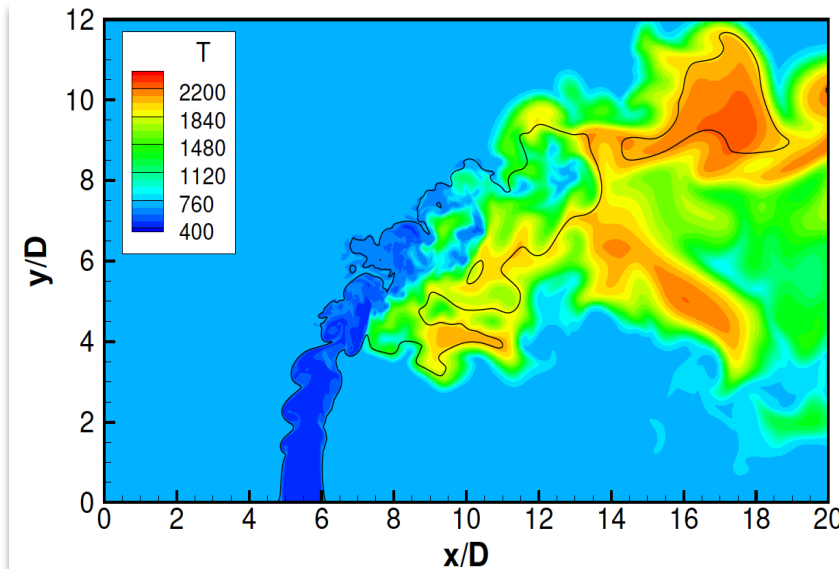
LES Combustion Modeling

- LES flamelet-based combustion model



LES Combustion Modeling

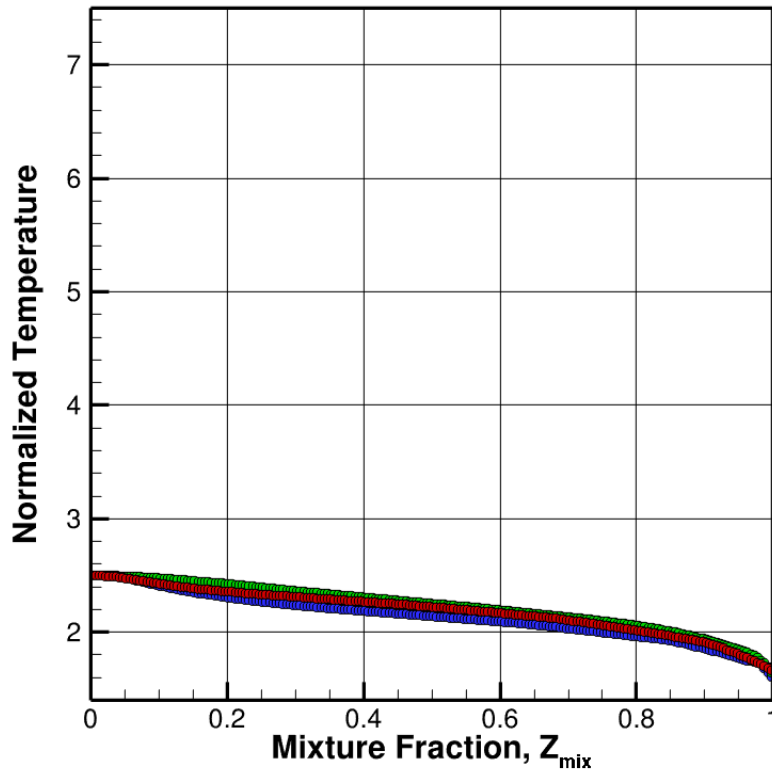
- Flamelet-structure in turbulent reacting flows
 - Analysis Tools: DNS-database¹ of reacting jet-in-cross-flow
 - Fuel: N₂-diluted H₂-jet, 350 K
 - Oxidizer: Air, 750 K
- Extract instantaneous **local flamelet structure** from DNS-database



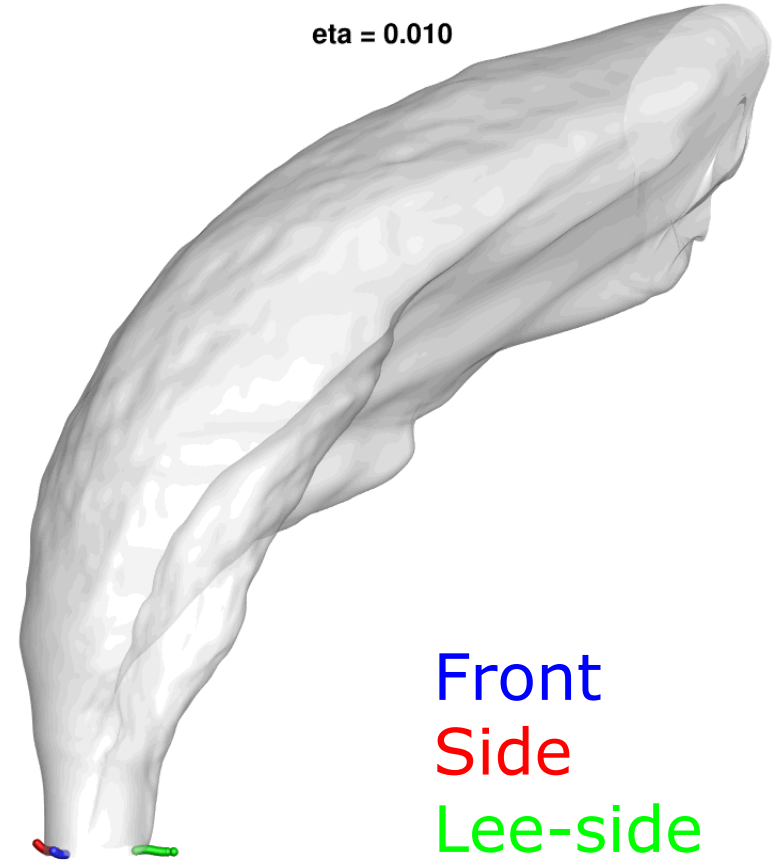
LES Combustion Modeling

- Evolution of 1D-flamelet-elements in JICF

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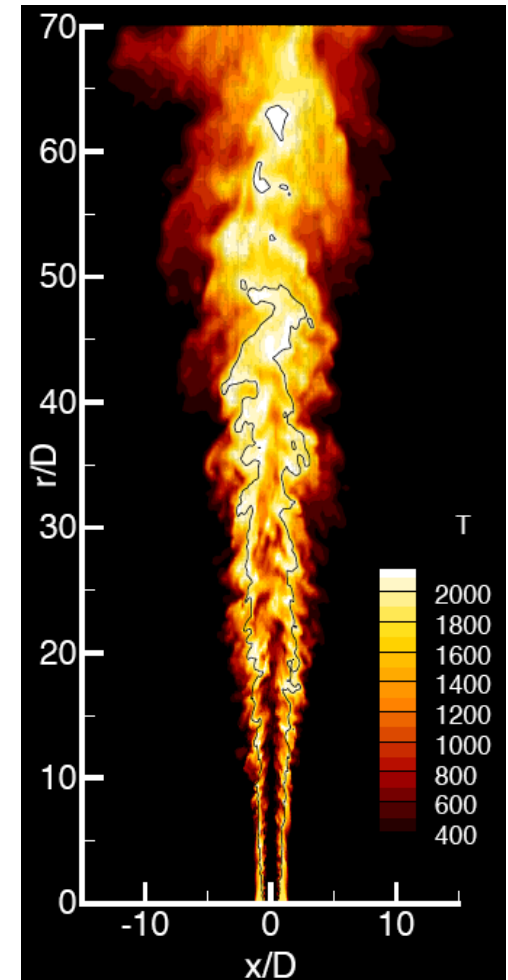


eta = 0.010



LES Combustion Modeling

- LES Flamelet-based combustion models
 - Parameterization of combustion process in terms of **reduces set of scalars**
 - Account for detailed chemistry
 - Tabulation of reaction chemistry
 - Consideration of turbulence chemistry coupling



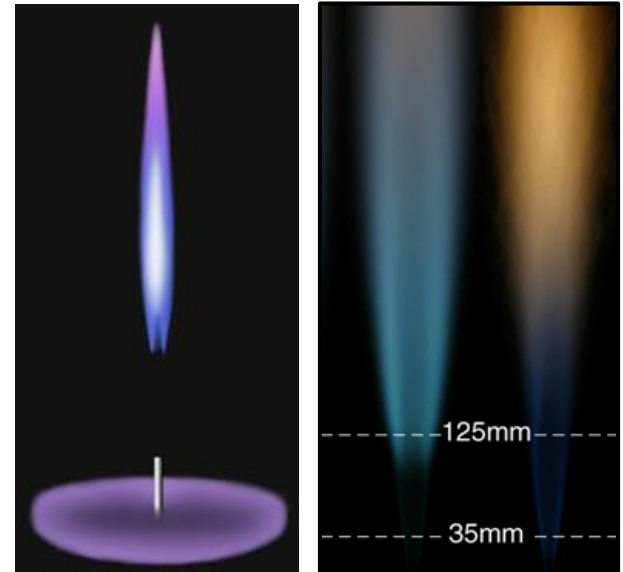


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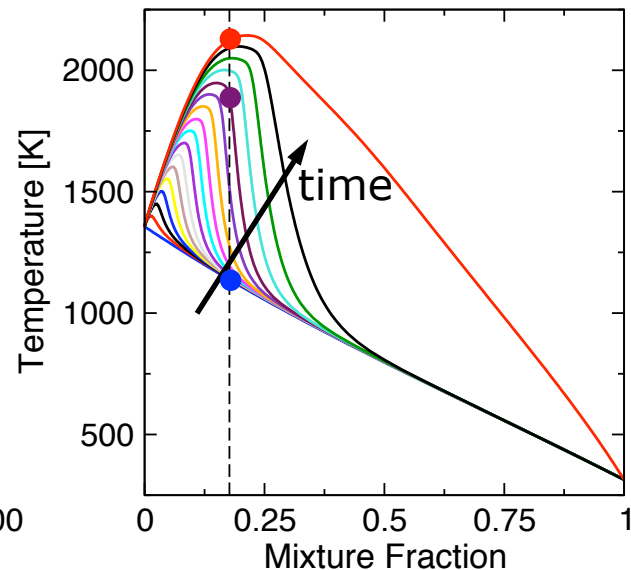
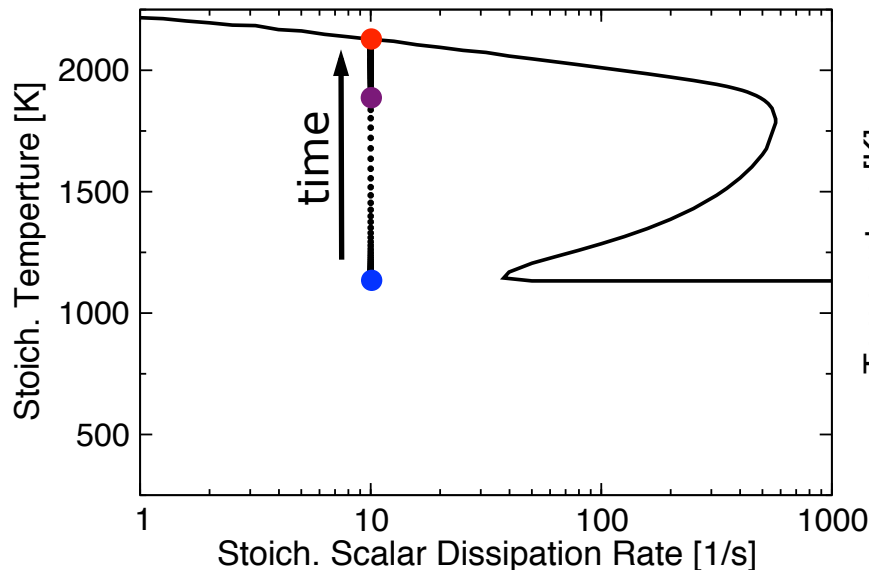
Autoignition in Turbulent Flames

- Modeling challenges in predicting autoignition in turbulent flames
 - Autoignition is **transient process**; requires accurate description of **temporal flame-evolution**
 - Flame stability and ignition dynamics strongly dependent on scalar mixing and **flame/turbulence interaction**
- Modeling approach¹
 - Autoignition requires consideration of transient species formation, described by **unsteady flamelet equations**
 - Turbulence/chemistry interaction: **Presumed PDF-closure** to consider effects of subgrid-mixing and unresolved flame structure



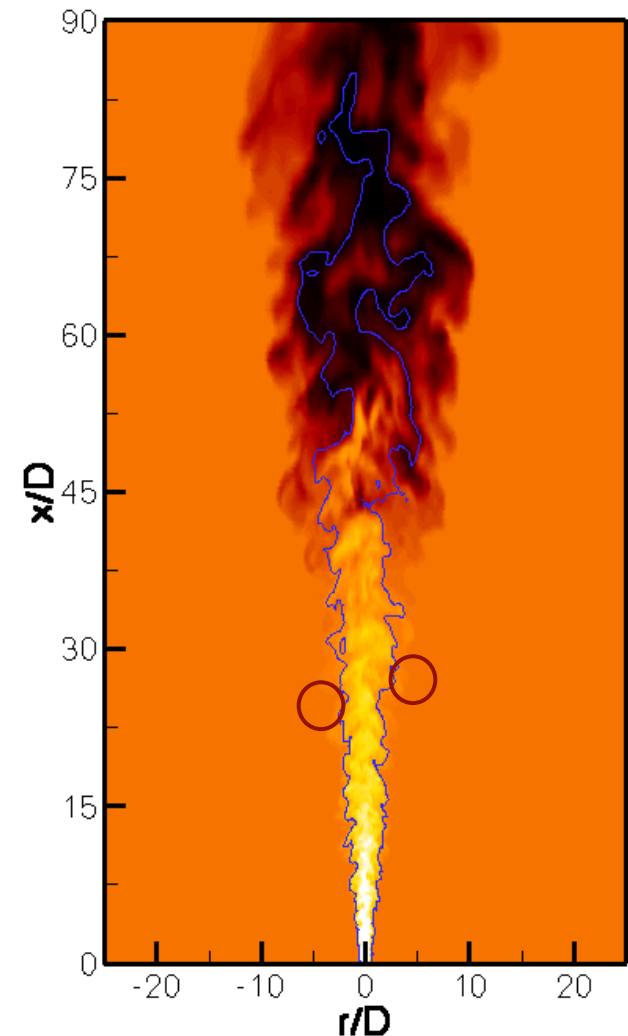
Autoignition in Turbulent Flames

- Conditions for flame-ignition in diffusion flames
 - Autoignition is transient process
 - Sufficiently low scalar dissipation rate
 - Flame ignition occurs under conditions corresponding to “most-reactive mixture”
 - Build-up of radical pool through chain-branching reaction

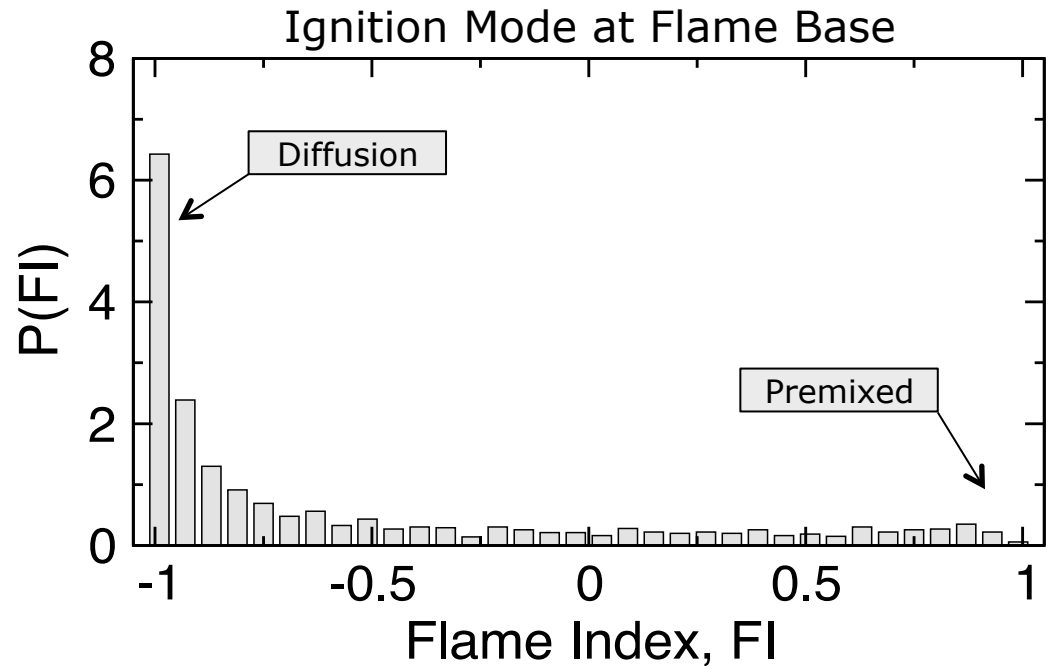
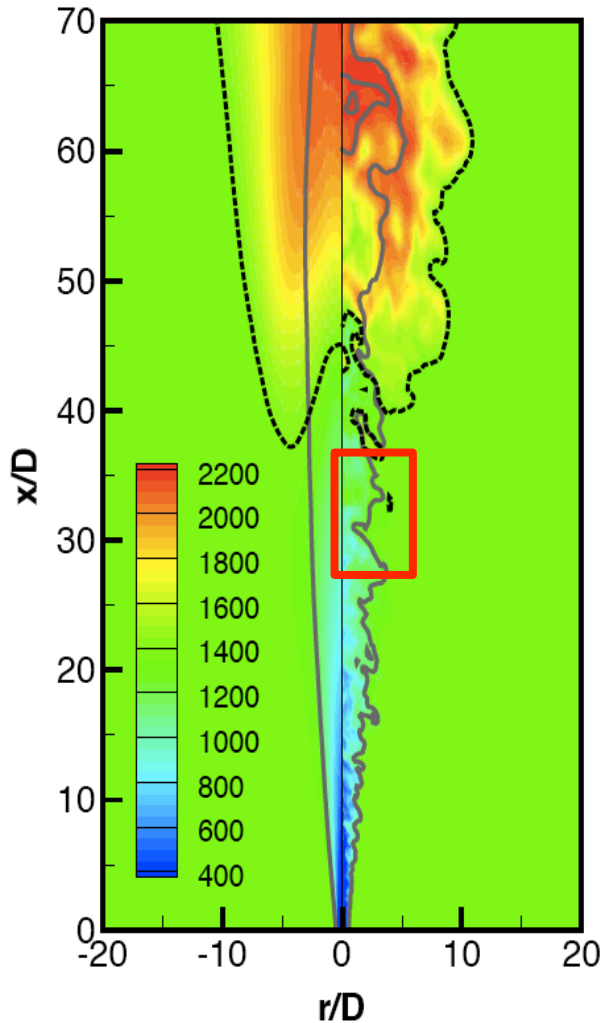


Autoignition in Turbulent Flames

- Experimental configuration
 - Lifted flame in vitiated co-flow
 - Fuel: methane/air 1:2
 - Co-flow temperature: 1350 K
 - Co-flow composition from premixed H_2 -Air reaction product
- Computational setup
 - Grid: 2.5 Mio grid points
 - Reaction Chem.: GRI 2.11, (also used GRI 3.0, USC-mech II)
 - 5-dimensional chemistry table with grid-refinement



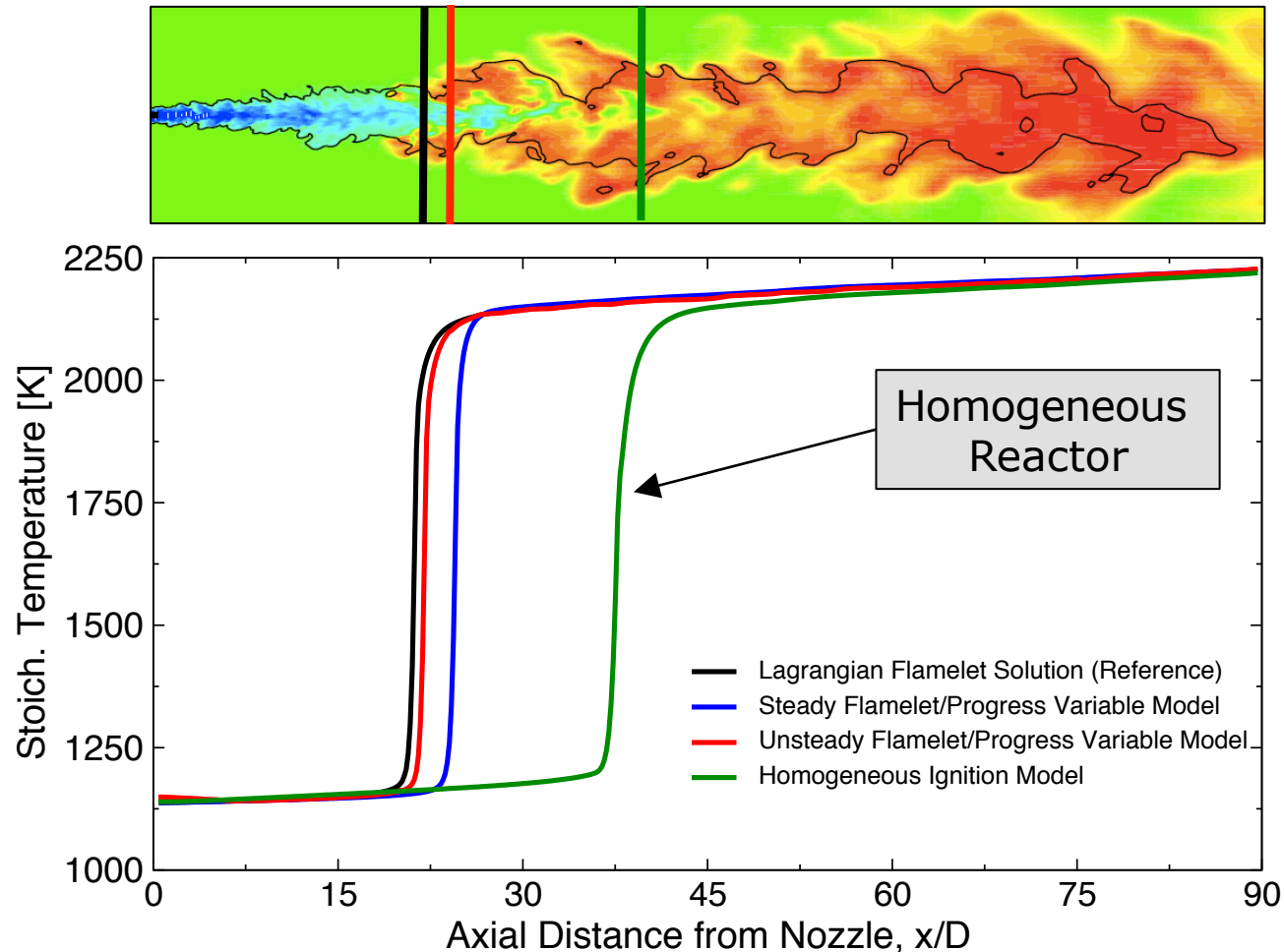
Autoignition in Turbulent Flames



- Ignition conditions: **low-strain** region at most-reactive mixture composition
- Ignition occurs primarily in diffusion regime
- Location of flame-base controlled by **HO_2 -radical pool** that is formed upstream of flame

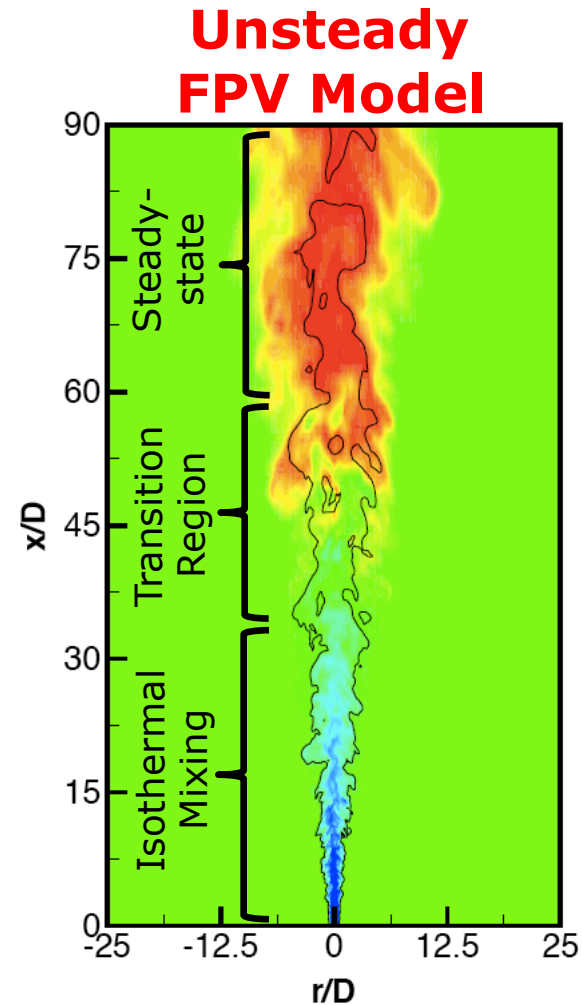
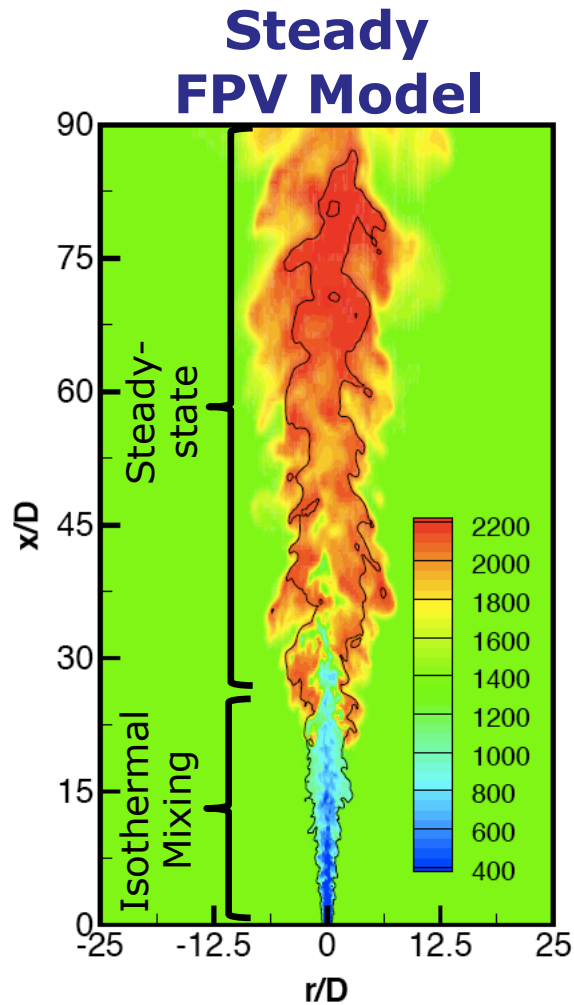
Autoignition in Turbulent Flames

- Effects of turbulence and scalar mixing



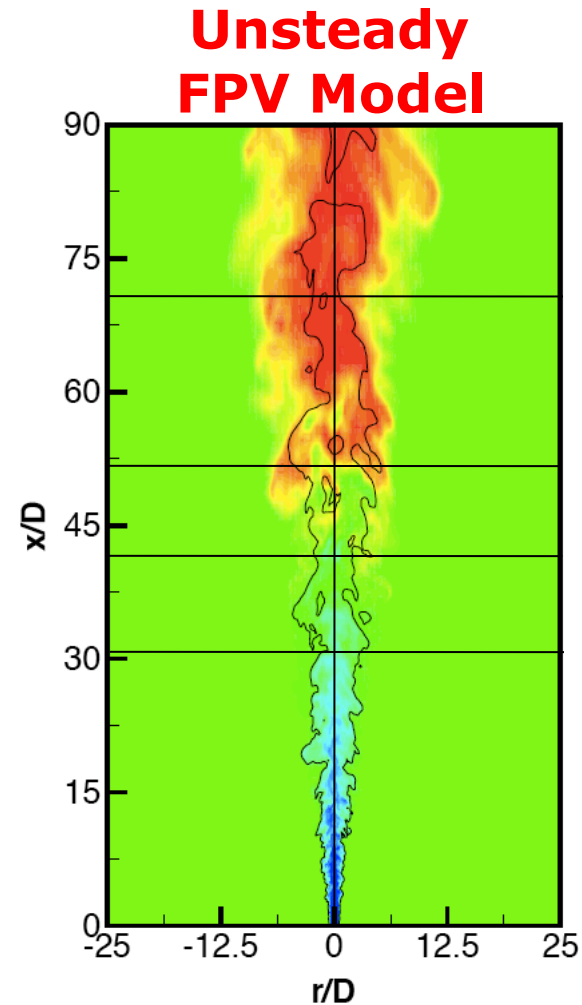
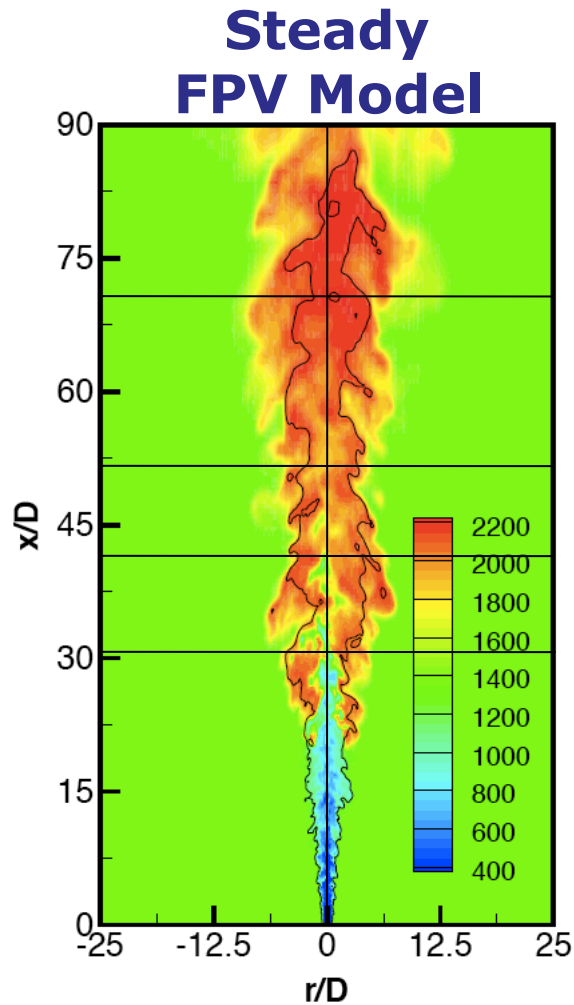
Autoignition in Turbulent Flames

- Instantaneous temperature field



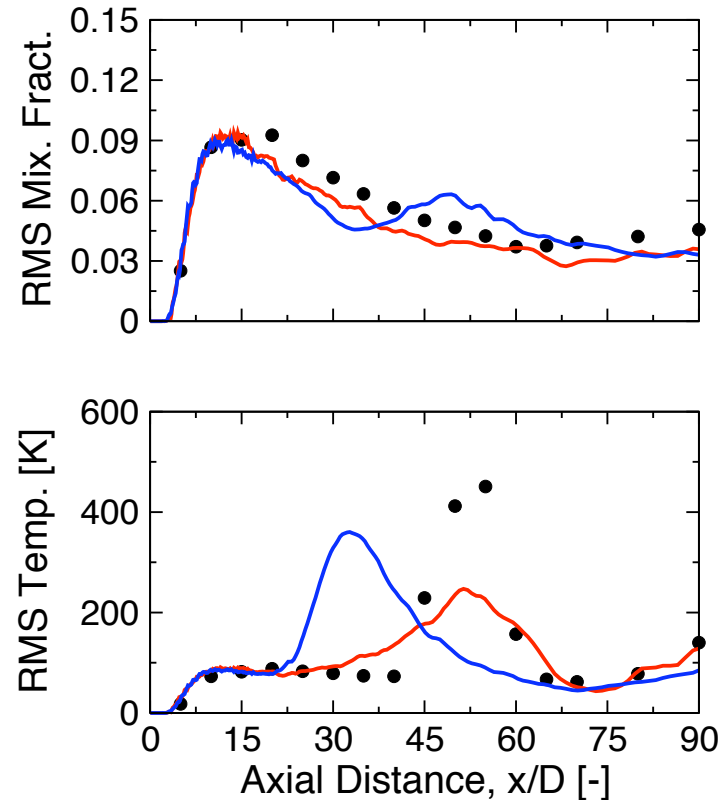
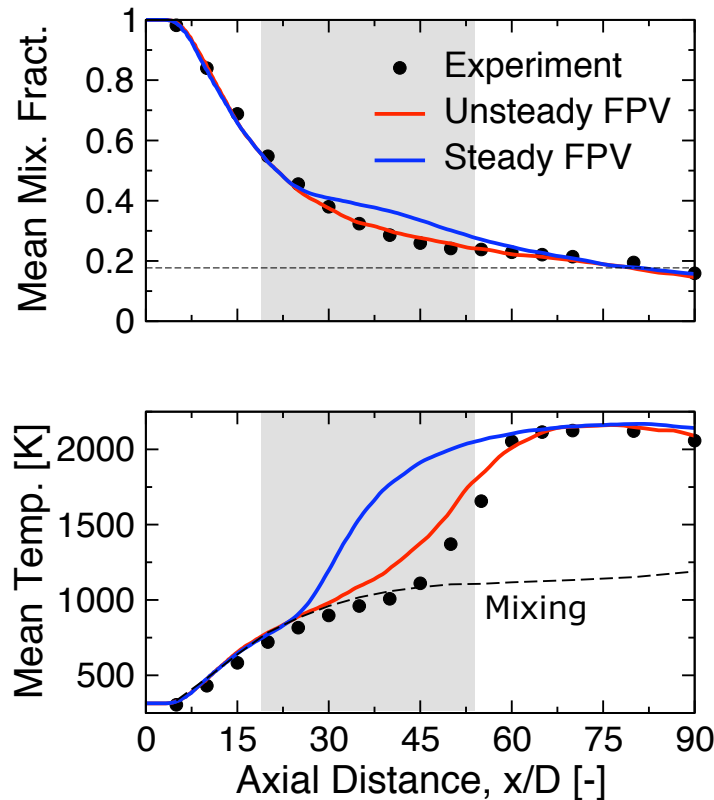
Autoignition in Turbulent Flames

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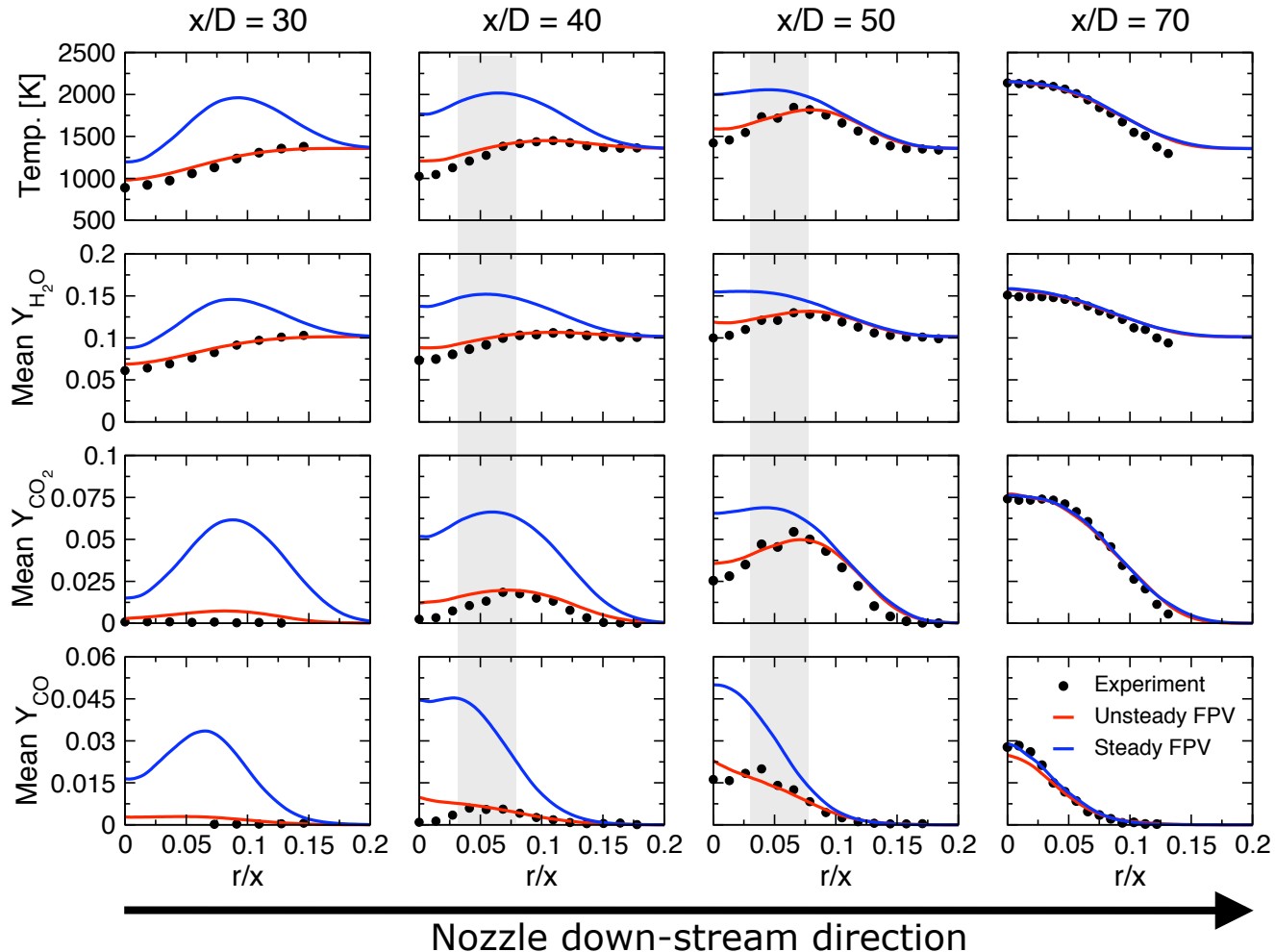
Autoignition in Turbulent Flames

- Centerline profiles



Autoignition in Turbulent Flames

- Radial profiles





Summary and Conclusions

- LES-modeling of lifted vitiated flames
- Key modeling components
 - Transient flame evolution
 - Accurate description of turbulent mixing and scalar dissipation rate
- Combustion-physical insights
 - Transient flame evolution
 - Identified **significance of flame/turbulence** interaction

→ Homogeneous reactor-model under-predicts ignition onset



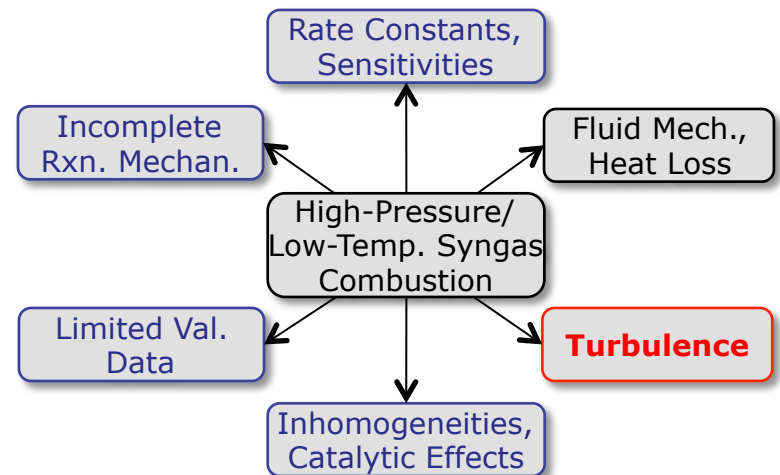
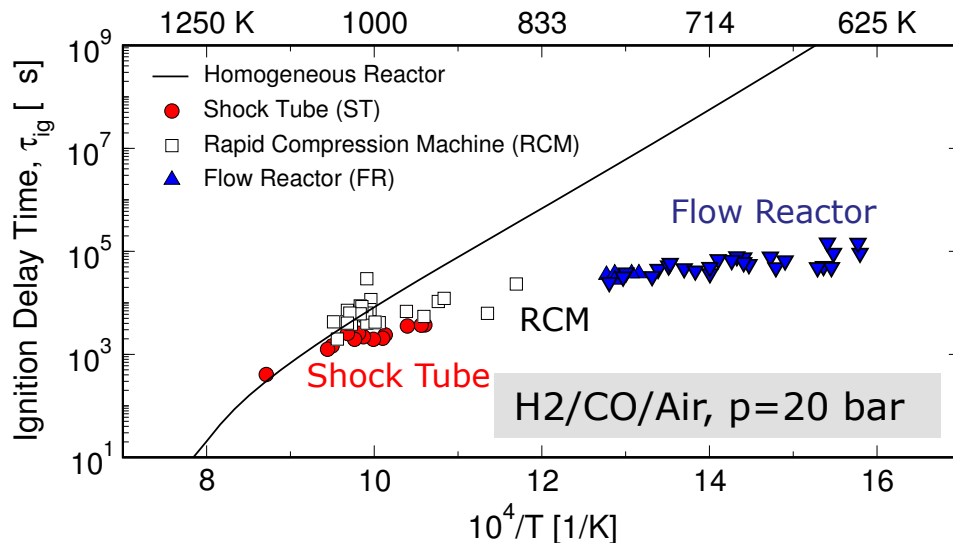
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Turbulent Inhomogeneities and Facility Effects

- Question: Can we apply “lessons-learned” from LES simulations to characterize experimental facilities?
 - Shock-tubes
 - Flow-reactors
 - Rapid compression machines

- Source of non-idealities in experimental facilities^{1,2,3}





- Research Objectives

- Use high-fidelity simulation and non-equilibrium formulation to isolate parametric contributions of non-idealities in experimental facilities
- Research emphasis
 - Identify **parametric sensitivities**
 - Reconcile observed differences between experiments and detailed model-formulations
- Facilities
 - Shock-tube
 - Flow-reactor
 - Rapid compression machine

Turbulent Inhomogeneities and Facility Effects

Shock-Tube



- Non-ideal processes in shock-tubes

1. *Non-ideal rapture of diaphragm*[#]

- Finite opening time of diaphragm
- Contribution to shock attenuation: 30%

2. *Boundary layer growth*^{\$}

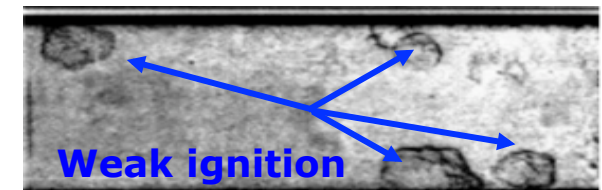
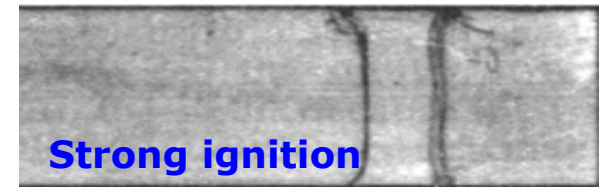
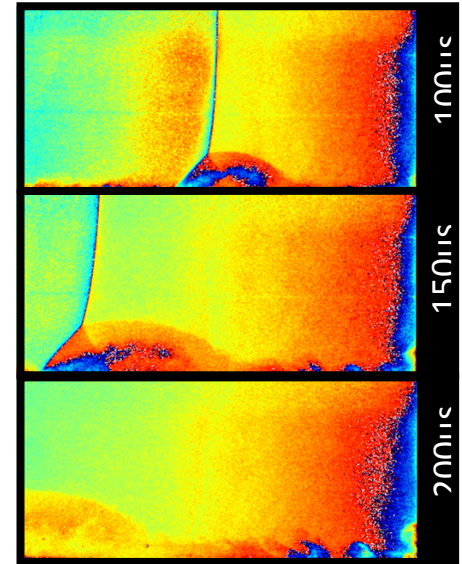
- Formation of viscous boundary layer behind initial shock

3. *Shock reflection and bifurcation*[%]

- Lift-off of boundary layer resulting in formation of separation region

4. *Inhomogeneous ignition and weak-to-strong ignition transition*^{\$}

- Ignition proceeds as multi-dimensional heterogeneous process



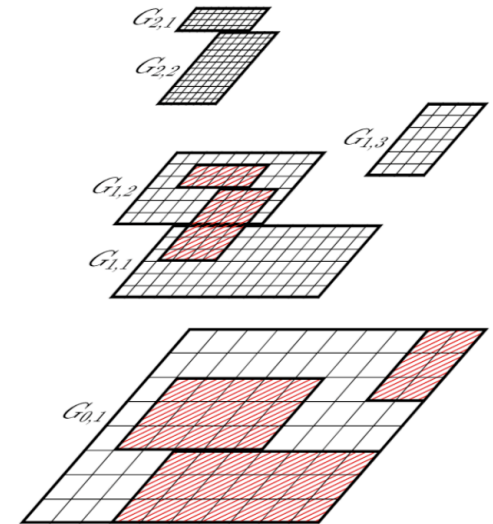
Turbulent Inhomogeneities and Facility Effects

Shock-Tube

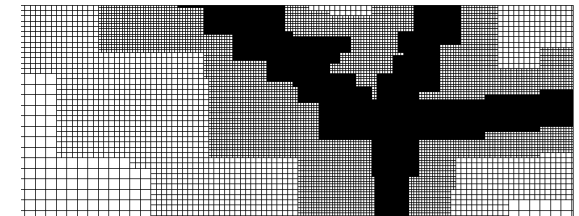


- Modeling challenges in simulating shock-tubes
 - Disparity of spatial and temporal scales

$$\underbrace{\frac{1}{150 \text{Re}_\tau^{2/7}} L}_{\text{Geometric shock-tube domain}} \sim \frac{1}{\text{Re}_\tau} \delta \sim \delta_v \sim \underbrace{\frac{\text{Re}_\tau M}{M_t}}_{\text{Shock Thickness}} \xi$$



- Solution method: Adaptive mesh refinement
 - AMR exploits multiscale nature of hydro-dynamic problem by locally adjusting computational effort to maintain uniform level of accuracy^{#, \$}



- Shock-bifurcation

- Simulation of Ar-diluted H_2/O_2 mixture at 5 and 10 bar pressure

- Relevant condition for weak and strong ignition regime

- Adiabatic and isothermal wall conditions

- Shock tube setup

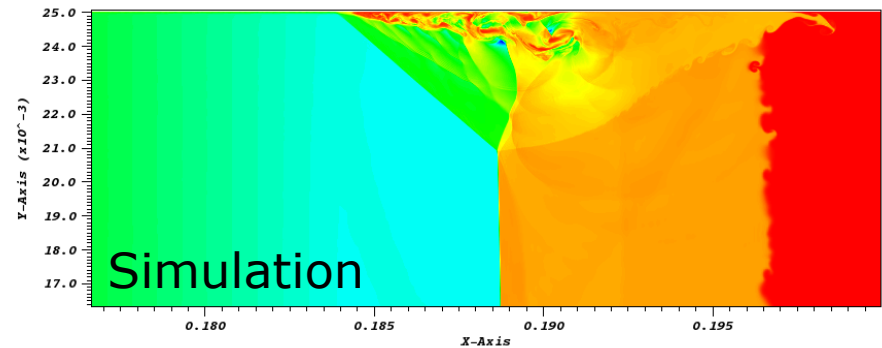
- Length: 1m
 - Diameter: 5 cm
 - Helium in driver section

- Target condition:

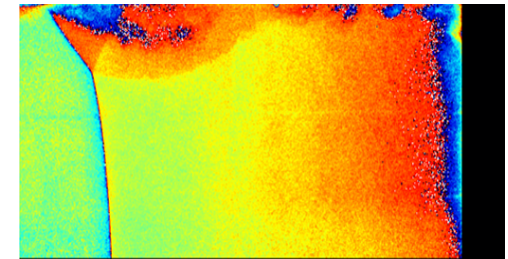
- $T_5=1100$ K, $p_5=10$ bar

- Chemical mechanism:

- Burke et al.¹ (2011)



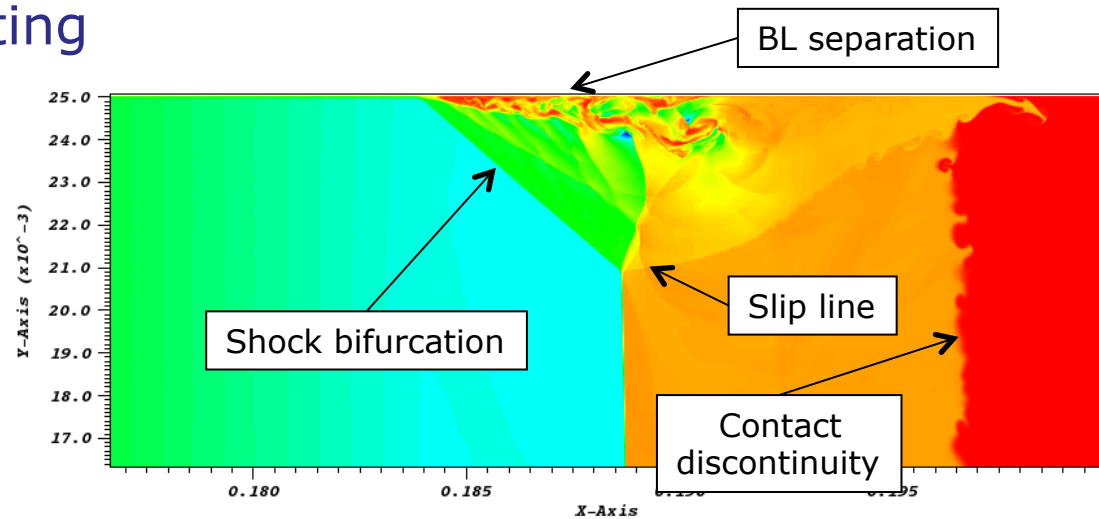
Experiment²



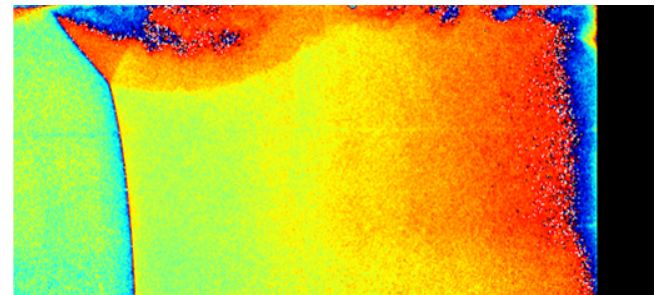
Results: Shock Bifurcation

- Shock-bifurcation

- Instantaneous temperature evolution shows rich flow-field structure: Boundary layer separation, Shock-bifurcation, Boundary heating



Toluene PLIF Measurements#

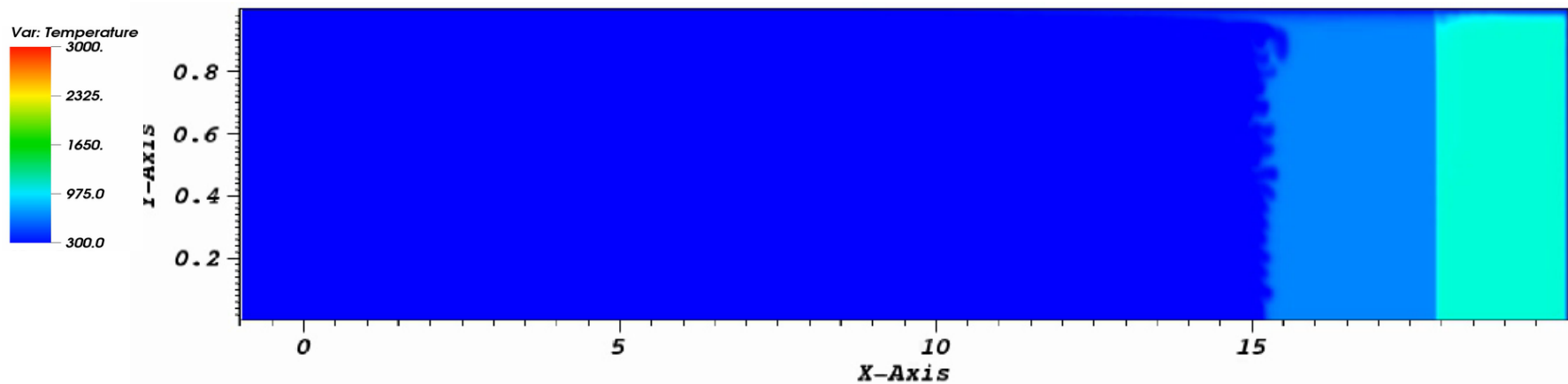


Turbulent Inhomogeneities and Facility Effects

Shock-Tube

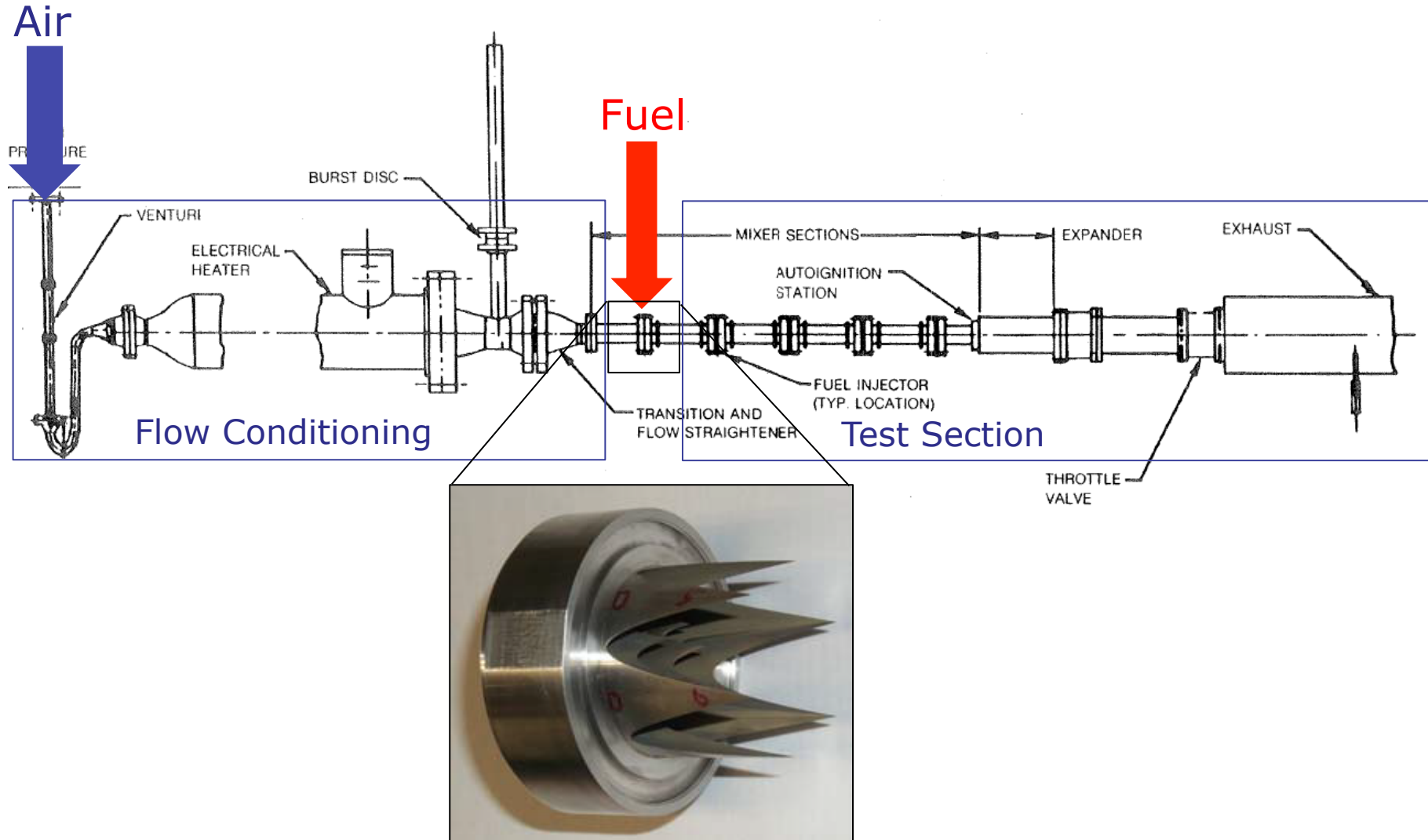


- Ignition
 - Isothermal wall

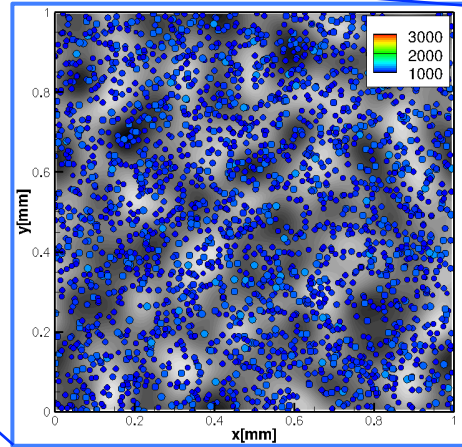
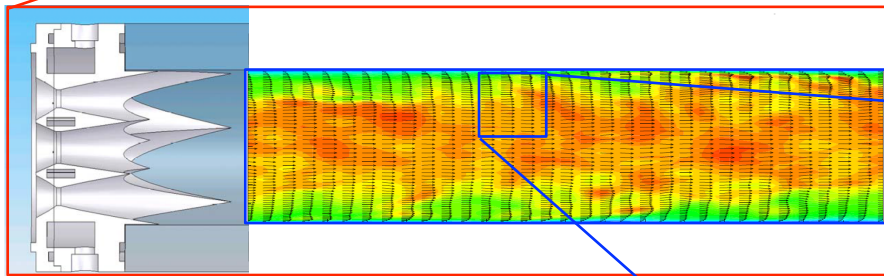
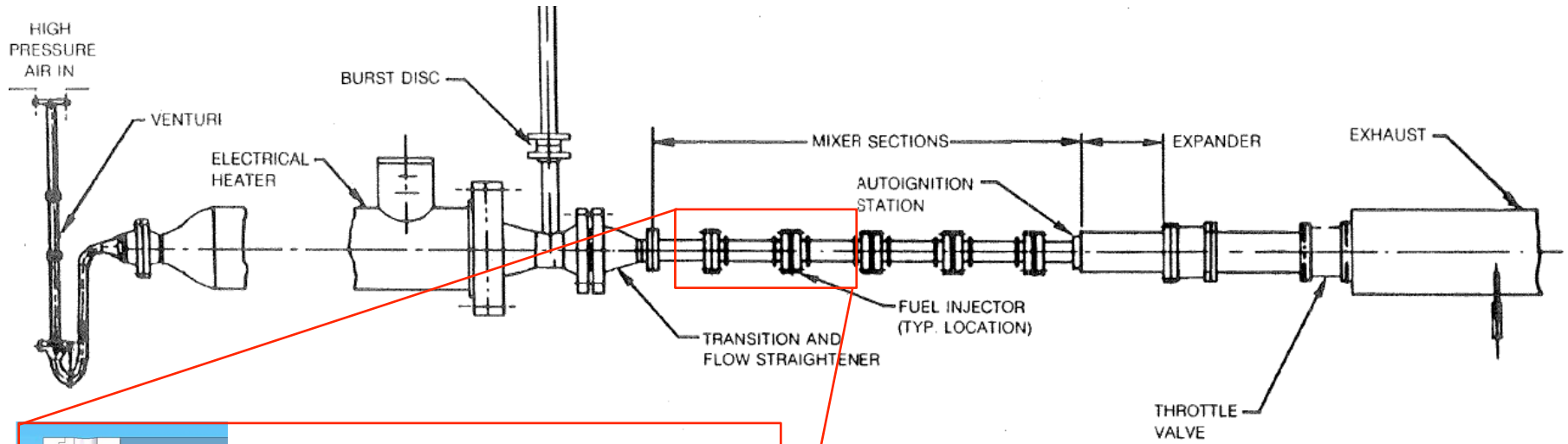


- Observations:
 - Ignition is initiated at end-wall
 - Flame propagation towards unburned mixture (region of favorable pressure gradient)
 - non-homogeneous ignition

Turbulent Inhomogeneities and Facility Effects Flow-Reactors



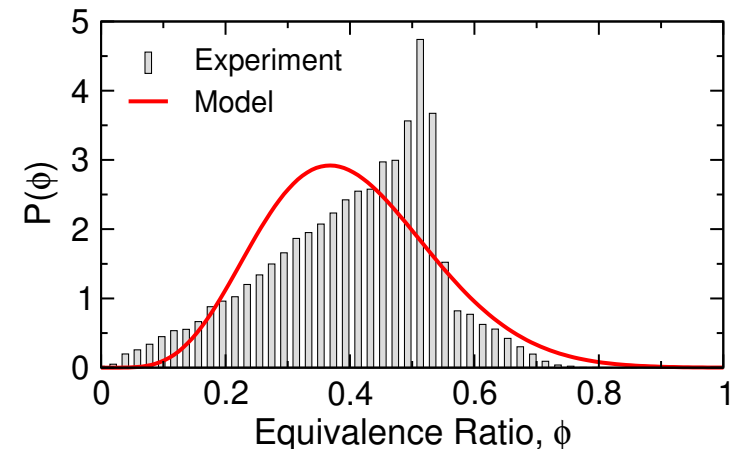
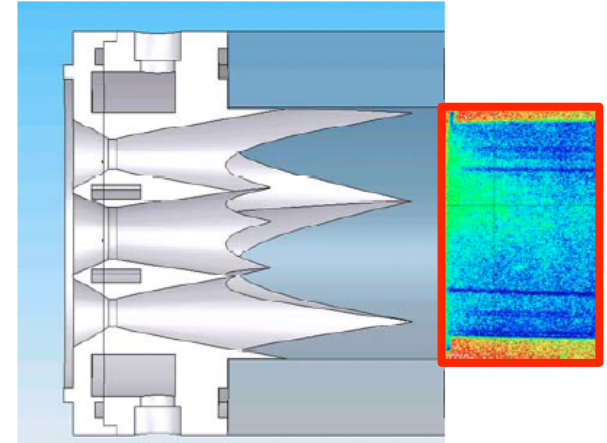
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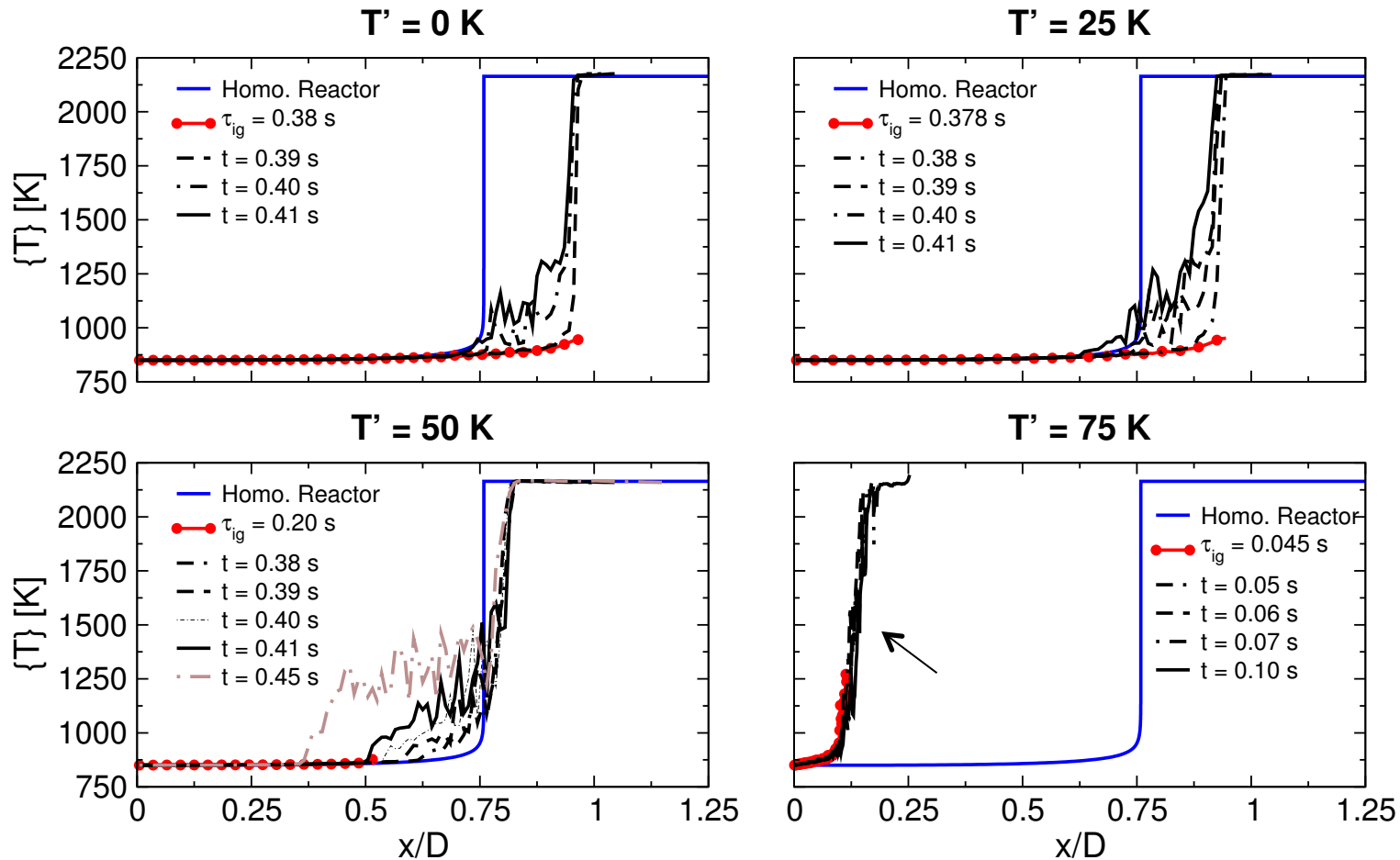
- Experimentally observed stochastic ignition suggests sensitivity to initial conditions
 - Mixture composition
 - Temperature
 - Unsteady heating
 - Wall-heat losses
 - Temp-difference btw. fuel and oxidizer
- Consider inhomogeneities
 - **Equivalence ratio**: sample from experimentally determined beta-distribution
 - **Temperature fluctuations**: Sample from Gaussian with specified T'
- Use fully-developed turbulent pipe-flow at $Re = 10^4$



Turbulent Inhomogeneities and Facility Effects Flow-Reactors



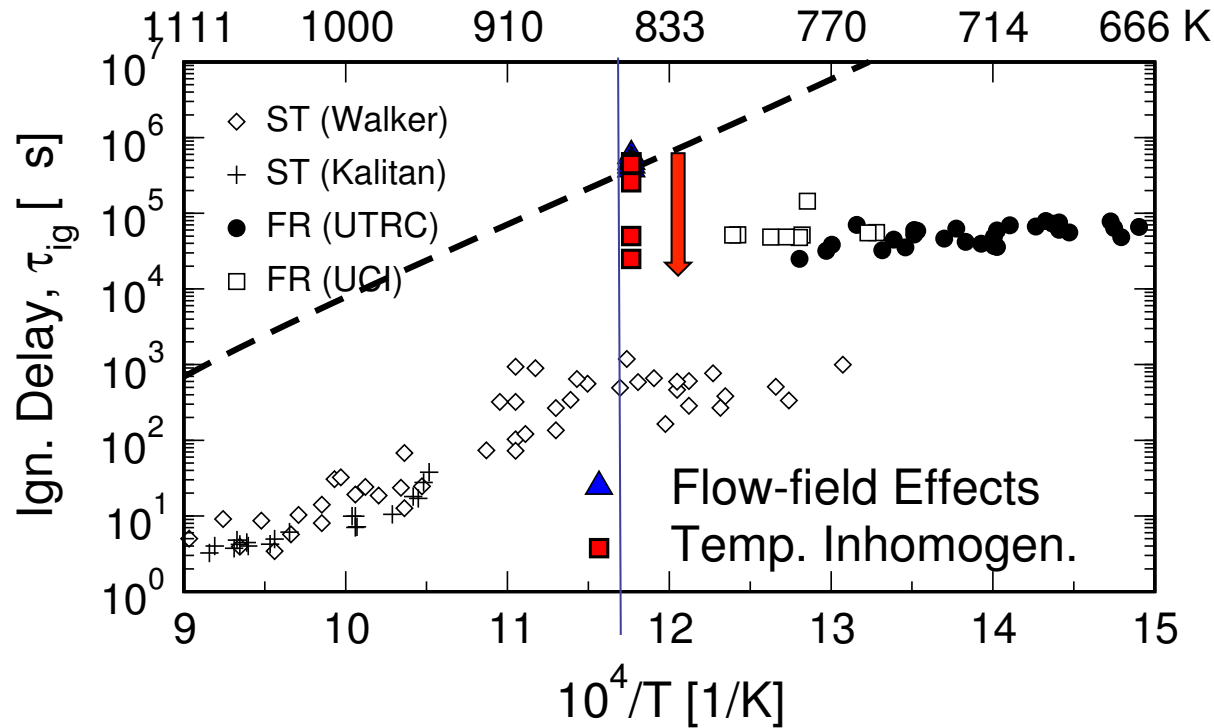
- Mixture variation: $\phi=0.4$; $\phi'=0.135$
- Temperature variation: $T=850$ K; $T' = \{0, 25, 50, 75\}$ K



Turbulent Inhomogeneities and Facility Effects Flow-Reactors



- Mixture variation: $\phi=0.4$; $\phi'=0.135$
- Temperature variation: $T=850$ K; $T' = \{0, 25, 50, 75\}$ K





Summary and Conclusions

- Turbulence/chemistry coupling processes
 - Increased relevance for low-Damkohler/high-Karlovitz combustion processes: oxygen-diluted comb.; autoignition; preheat-comb.
 - Turbulence promotes mixing, exchange of radicals and enthalpy
 - Ignition occurs at preferred sites: “most-reactive” mixture and regions of low strain
- Validated high-fidelity LES combustion models have been developed and are available to accurately capture ignition processes
 - Models rely on experimental data
- Simulations can assist and complement experimental investigations
 - Identify experimental sensitivities
 - Guide potential modifications to mitigate facility effects
 - Reconcile discrepancies btw. experiments and theory
 - **Example:** Turbulence/chemistry coupling in shock-tubes and flow-reactors